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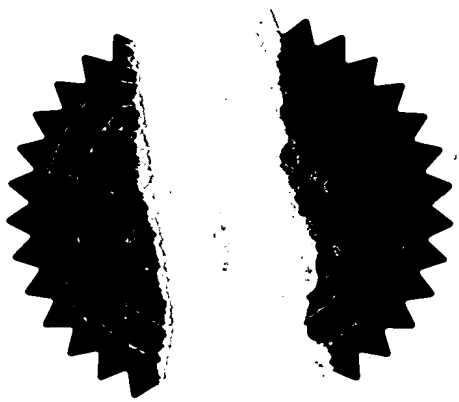
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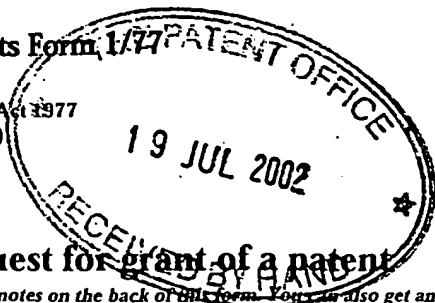


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Dated 1 July 2003

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1/77

22JUL02 E734901-1 D00571  
P01/7700 0.00-0216914.2

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The Patent Office

Cardiff Road  
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1. Your reference

SG/P9085GB

2. Patent application number

0216914.2

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19 JUL 2002

3. Full name, address and postcode of the or of each applicant (underline all surnames)

Air Products and Chemicals, Inc.  
7201 Hamilton Boulevard  
Allentown  
Pennsylvania 18195-1501  
USA

Patents ADP number (*if you know it*)

If the applicant is a corporate body, give the country/state of its incorporation

USA (Delaware)

5558366001

4. Title of the invention

PROCESS AND APPARATUS FOR TREATING A  
FEED GAS

5. Name of your agent (*if you have one*)

W. H. Beck, Greener & Co.

"Address for service" in the United Kingdom to which all correspondence should be sent (*including the postcode*)

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Patents ADP number (*if you know it*)

323001

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Country

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Claim(s) 4

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Process and Apparatus for Treating a Feed gas

5           This invention relates to a process and apparatus for treating a feed gas. In particular, the invention relates to a thermal swing adsorption (TSA) process using at least three adsorption beds for removing or at least reducing the level of a component in a feed gas to render it suitable for downstream processing and apparatus for use in the  
10   process. The invention is especially useful in removing components from a feed gas on a large scale where conventional processes and apparatus are not suitable for use.

          Where a feed gas is to be subjected to downstream processing, it may often be desirable or necessary to remove certain components from  
15   the feed gas prior to such processing. As an example, high boiling materials for example water and carbon dioxide which may be present in a feed gas, for example air, must be removed where the mixture is to be subsequently treated in a low temperature, for example cryogenic, process. If relatively high boiling materials are not removed, they may  
20   liquefy or solidify in subsequent processing and lead to pressure drops, flow difficulties or other disadvantage in the downstream process.

          Hazardous, for instance explosive, materials are suitably removed prior to further processing of the feed gas so as to reduce the risk of build-up in the subsequent process thereby presenting a hazard. Hydrocarbon  
25   gases, for example acetylene, may present such a hazard.

          In an air separation process, the gas is typically compressed using a main compressor (MAC) followed by cooling and removal of the thus condensed water in a separator. The gas may be further cooled using for example refrigerated ethylene glycol. The bulk of the water is removed in  
30   this step by condensation and separation of the condensate. The gas is then passed to an adsorption process where the components to be removed from the feed gas are removed by adsorption and then to an air

separation unit. In treating air, water is conventionally removed first and then carbon dioxide by passing the feed gas through a single adsorbent layer or separate layers of adsorbent selected for preferential adsorption of water and carbon dioxide prior to feeding the treated air to a downstream separation process.

Several methods are known for removing an undesired component from a feed gas by adsorption on to a solid adsorbent including temperature swing adsorption (TSA) and pressure swing adsorption (PSA), thermal pressure swing adsorption (TPSA) and thermally enhanced pressure swing adsorption (TEPSA). Conventionally in such methods, two adsorbent beds are employed in a parallel arrangement with one being operated for adsorption while the other is off-line and being regenerated and then the roles of the beds are periodically reversed in the operating cycle. The adsorption bed is said to be "on-line" during the adsorption step.

In a TSA process, the adsorption step generates heat of adsorption causing a heat pulse to progress downstream through the adsorbent bed. The heat pulse is allowed to proceed out of the downstream end of the adsorbent bed during the feed or on-line period. After adsorption, the flow of feed gas is shut off from the adsorbent bed which is then depressurised. The adsorbent is then exposed to a flow of hot regeneration gas, typically a waste stream or other gas from the downstream process, which strips the adsorbed materials from the adsorbent and so regenerates it for further use. Regeneration conventionally is carried out in a direction counter to that of the adsorption step. The bed is then repressurised in readiness to repeat the adsorption step.

A PSA system typically involves a cycle in which the bed is on-line, and then depressurised, regenerated and then repressurised before being taken back on-line. Depressurisation involves releasing pressurised gas and leads to waste, generally known as "switch loss". In PSA systems, the pressure of the regeneration gas is lower than that of

the feed gas. It is this change in pressure that is used to remove the adsorbed component from the adsorbent. However, cycle times are usually short, for example of the order of 15 to 30 minutes, as compared with those employed in a TSA system, which may be for example of the order of 2 to 20 hours. PSA therefore has certain disadvantages including unacceptable switch loss due to the relatively high frequency of switching between on-line operation and regeneration, especially in operating large capacity plant.

US-A-5656065 describes a PSA process that employs three beds operated in a phased cycle which aims to reduce switch loss and improve continuity of flow of the feed gas to a downstream process. The purpose of the third bed is to allow a process cycle in which a small flow of pressurised feed gas is fed to the bed undergoing repressurisation. Hence, the repressurisation step is relatively long but a reduction in the interruption of the treated gas to a downstream process is advantageously secured.

Thermal pressure swing adsorption (TPSA) is also suitable for removing components from a feed gas by adsorption. In a TPSA system an undesired component is typically adsorbed in a first zone in which an adsorption medium is disposed for example activated alumina or silica gel. A second undesired component is then adsorbed in a second zone. TPSA, utilises a two stage regeneration process in which one adsorbed component is desorbed by TSA and another is desorbed by PSA. A TPSA process is described in US-A-5885650 and US-A-5846295.

In thermally enhanced PSA (TEPSA), desorption occurs by feeding a regeneration gas at a pressure lower than the feed gas and at a temperature greater it and subsequently replacing the hot regeneration gas by a cold regeneration gas. The heated regeneration gas allows the cycle time to be extended as compared to that of a PSA system so reducing switch losses as heat generated by adsorption within the bed may be replaced in part by the heat from the hot regeneration gas. A TEPSA process is described in US-A-5614000.

TSA TPSA and TEP SA systems require the input of thermal energy and may require the use of insulated vessels, a regeneration gas preheater and an inlet end pre cooler and generally the high temperatures impose a more stringent and costly mechanical specification for the system. In operation, there is extra energy cost associated with using the preheater.

By the term "thermal swing adsorption" we mean adsorption processes and apparatus for operating the process in which thermal energy is input to regenerate the adsorbent and includes TPSA and TEP SA processes in addition to TSA unless otherwise stated.

TSA apparatus typically comprises a pair of adsorber vessels, both containing adsorbent. The vessels may be of any conventional type including the vertical, horizontal and radial type.

Conventional purification in a TSA process, especially where larger vessels are employed, may be problematic because the flow characteristics of the gas being processed may place limitations due to the need to avoid undue fluidization of the adsorbent bed and unacceptable pressure drop. In addition complex design of vessel geometry to address these issues, especially to accommodate large flows, may themselves introduce further problems. Accordingly, large vessels present certain problems and there are practical limits for their use.

Radial flow adsorbers have been employed to reduce problems with flow but they are typically more expensive than vertical and simple horizontal vessels. For radial beds, a higher ratio of bed height to bed diameter is required to gain a higher flow. In addition the bed's effective thickness is typically limited by the diameter which may itself be limited by constraints in transporting the adsorption vessel in manufacture and assembly of the plant. Moreover, the bed size is limited by the need to avoid a large pressure drop and lack of uniformity of flow.

In a horizontal bed, a reduction in bed thickness and increase in the ratio of effective bed length to diameter also has practical limits and long horizontal beds are therefore undesirable.

To increase capacity, a "four bed" configuration may be used in a TSA process in which two beds are on line with two beds being regenerated at the

same time and the regenerated beds then being placed on-line and the other, exhausted beds being regenerated to provide a high throughput. The four beds are typically are operated as two pairs of beds and the phasing of the adsorption/regeneration cycle of the two pairs need not be co-ordinated. In this way four simple vessels having a conventional geometry and design may be used to avoid difficulties of pressure drops and transportation which could be encountered if larger scale equipment were to be employed. This approach however requires significant capital investment and adds to the complexities of design of a large scale separation unit.

10 We have now found that technical problems such as undesirable fluid flow, bed fluidisation and unacceptable pressure drop and economic and practical problems including cost, design complexity and difficulties in transporting large-scale apparatus may be reduced or avoided by operating a TSA process using at least three adsorption zones in which, 15 in use, at least two of the zones are always on-line. Each of the zones repeatedly passes through the cycle of adsorption and regeneration, the each zone being at a point on the cycle which is out of phase with the other zones so that at any given time at least two zones are adsorbing a component of the feed gas and a third zone is being regenerated and is 20 brought on-line as or before one of the zones in the adsorption phase is taken off-line to be regenerated. By employing a TSA process, characteristics inherent in a PSA process are also avoided.

A first aspect of the invention provides a process for the reduction of the level of a component in a feed gas comprising passing the feed 25 gas to at least three parallel thermal swing adsorption zones, each zone containing an adsorbent and being operated in an adsorption cycle which comprises an adsorption step to remove or to reduce the level of the component from the feed gas, depressurisation of the adsorption zone, a regeneration step to desorb the adsorbed component and 30 repressurisation of the adsorption zone, wherein the adsorption cycle of each zone is phased with respect to that of the other zones so that at any



point during the adsorption cycle, the number of zones in the adsorption step is greater than the number of zones not in the adsorption step.

In the regeneration step, a regeneration gas is suitably fed to the adsorption zone being regenerated so as to desorb the adsorbed component thereby regenerating the zone for a subsequent adsorption step in a new adsorption cycle.

Advantageously, a high process throughput may be secured as compared to prior art processes for a given scale of apparatus and avoids the disadvantage of higher cost, flow fluctuations and pressure drop associated with the use of larger scale equipment to achieve a comparable throughput.

The invention provides in a second aspect, thermal swing adsorption apparatus for conducting thermal swing adsorption of a component in a feed gas, the apparatus comprising at least three parallel thermal swing adsorption zones adapted to receive an adsorbent bed and means for controlling the flow of the feed gas through the at least three zones such that each bed undergoes repeated adsorption cycles which cycle comprises an adsorption step to remove or to reduce the level of the component from the feed gas, depressurisation of the zone, a regeneration step to desorb the adsorbed component and repressurisation of the adsorption zone, and wherein the adsorption cycle of each zone is phased with respect to that of the other zones so that, in use, the number of zones in the adsorption step is greater than the number of zones not in the adsorption step.

The regeneration step suitably comprises feeding a regeneration gas to the adsorption zone undergoing regeneration. The apparatus according to the invention also suitably comprises means for controlling the flow of a regeneration gas such that the regeneration step may be successively performed for each of the adsorption zones and a heater for heating the regeneration gas.

The means for controlling the flow of feed gas may comprise conduits for gas flow in or connecting the zones and connecting each bed to a source of the

feed gas and to an outlet from the apparatus for the gas treated by removal or reduction of the undesired component, valve means in the conduits operable to open and close respective ones of the conduits. It is especially preferred that the means for controlling the flow of gas comprises valve control means programmed to operate the valve means in sequence to produce the required adsorption cycles of operation.

The apparatus also suitably comprises means to control the flow of gas for regeneration, depressurisation and repressurisation.

In a preferred embodiment, the adsorption zone is defined by a conventional adsorption vessel. Preferably the apparatus comprises three adsorption vessels.

As a practical advantage, the use of three adsorption vessels each having half the capacity of each of two larger vessels requires about 25% less adsorbent than the two vessels of twice the capacity. In operating the two bed, large vessel system conventionally, one bed at a time would be on-line. However, in operating the three vessel system, two of the three vessels would be on-line at a given time providing a comparable throughput. Moreover, by virtue of splitting the feed gas into two streams to feed both vessels, the size of tubing and valves required in the plant will be smaller and provide significant cost benefits as compared to conventional apparatus because typically the cost of valves increases greatly with size.

Preferably, the process according to the invention is carried out in the apparatus according to the invention.

Suitably, at least two zones are in the adsorption step and at least one is in the regeneration step at any point during the adsorption cycle. Preferably, the number of zones in the adsorption step at any point during the adsorption cycle is constant so as to provide advantageously a relatively constant throughput of the feed gas and reducing fluctuations in flow volume in a downstream process. Optimally, the number of zones in the adsorption step at any point during the cycle is one fewer than the

total number of adsorption zones so that, at any point only one zone is in the regeneration step so as to maximise throughput of the feed gas.

In a preferred embodiment the adsorption cycle of each zone commences at a different time to the commencement of the adsorption cycle of the other zones and for all the adsorption zones is substantially the same duration. More preferably, in addition, the adsorption step for each zone is substantially the same duration as that for the other zones. More preferably, the ratio of the duration of the adsorption step to the adsorption cycle is not less than the ratio of one less than the number of adsorption zones to the number of adsorption zones.

For reference, the adsorption cycle herein is considered to start with the adsorption step and then to be followed by depressurisation, the regeneration step and repressurisation.

The feed gas comprises a desired component and a component to be removed from the feed gas by adsorption. For example the feed gas may contain carbon dioxide and water. The feed gas may be natural gas or synthetic gas and in a preferred embodiment, the feed gas is air. After treatment, the gas is suitably subjected to a downstream process of cryogenic separation especially for the recovery of oxygen and/or nitrogen.

Where the feed gas contains carbon dioxide and water, it is suitably treated by contacting with a first adsorbent so as to remove the water prior to removal of carbon dioxide suitably on a second adsorbent. Suitable adsorbents include alumina, silica gel, activated alumina, impregnated alumina, and molecular sieves, for example zeolite of the X type, A type and LSX. Preferably the zeolite has a silicon to aluminium ratio of 1.0 to 1.25. The water adsorbent material is preferably silica gel, activated alumina or impregnated alumina and the carbon dioxide adsorbent material may be a molecular sieve for example, a zeolite. The zeolite may be bound or binderless. Preferably, the zeolite is sodium exchanged zeolite X, sodium exchanged zeolite Y or calcium exchanged

zeolite X. More than one adsorbent may be employed in a single bed, for example as separate layers, as desired.

Preferably, the water adsorbent and carbon dioxide adsorbent are arranged in a composite bed with the carbon dioxide adsorbent downstream of the water adsorbent although separate beds may be employed if desired.

The TSA process according to the invention is preferably operated using at least three parallel flow paths and optimally the same number of flow paths as adsorption zones, so as to allow the process to be operated in a cyclical manner comprising adsorption and desorption with the separate flow paths being cycled out of phase to provide a pseudo-continuous flow of feed gas from the process through the at least three adsorption zones.

The feed gas is suitably fed to the adsorption step at a temperature of  $-50$  to  $80^{\circ}\text{C}$  and preferably  $0$  to  $60^{\circ}\text{C}$ , especially  $5$  to  $50^{\circ}\text{C}$ . Suitably the pressure of the feed gas is at least  $100000\text{ N/m}^2$ , preferably  $200000$  to  $4000000$  more preferably  $200000$  to  $3000000$  and desirably  $200000$  to  $2000000\text{ N/m}^2$ .

In the process, the feed gas is introduced into an adsorption zone and contacted with the adsorbent, suitably in the form of a bed. As the mixture passes through the adsorbent, the component(s) to be adsorbed are adsorbed and the remaining gas then passes out of the adsorption zone. During the process a front of the gas to be adsorbed forms in the adsorbent and passes through it. As desired, the adsorption step is then terminated and the adsorption zone is then heated and optionally subjected to a reduced pressure and is purged of the adsorbed gas during regeneration by feeding a regeneration gas to the zone.

The adsorption step is suitably operated in a conventional manner known to those skilled in the art.

Preferably, the regeneration gas comprises a gas recycled from a downstream process, for example a nitrogen-rich waste gas stream from an air separation plant which is dry and free of carbon dioxide. Preferred

regeneration gases include oxygen, nitrogen, methane, hydrogen and argon and mixtures thereof.

The regeneration of the adsorbent is suitably carried using a regeneration gas at a temperature above the bed adsorption temperature, suitably at a temperature of 0 to 400°C, preferably from 40 to 200°C.

Suitably, the regeneration pressure is 10000 to 2000000 N/m<sup>2</sup> and preferably 20000 to 1500000 N/m<sup>2</sup>. It is especially desirable that the regeneration pressure does not exceed 50 percent of the pressure of the feed gas.

Repressurisation may be effected by passing upstream, feed gas or downstream, treated gas through the bed to be regenerated. The repressurisation gas is at a higher pressure than the adsorption zone.

Preferably, the process is operated with a molar flow of regeneration gas to the feed gas of 0.05 to 0.8 more preferably 0.1 to 0.5.

Suitably, in a TSA process and a TPSA process, the feed gas is fed to the adsorption zone for a period of 6 to 1000 minutes and preferably 70 to 300 minutes. In a TEPsA process the feed gas is suitably fed to adsorption unit zone for a period of 10 to 150 minutes and preferably 20 to 80 minutes.

Advantageously, in use, where the adsorbent is free standing in a horizontal or vertical vessel, the fluid flow is suitably not more than 90% and desirably not more than 70% of the flow at which fluidisation of the bed occurs.

The present invention also allows independent feed gases which have a different characteristic to the other gases. Each feed gas may be of different composition or have different properties, for example flow, pressure, temperature and rate, on being fed to the adsorption cycle. In these circumstances, each adsorption zone is designed to take account of the most extreme conditions of the different feed stocks thereby enabling the different feeds to be cycled between each bed with regeneration in between.

The invention also provides in a preferred embodiment a thermal swing adsorption apparatus comprising at least three adsorption vessels, a feed gas inlet assembly in fluid communication with each vessel, an outlet assembly in fluid communication with the at least three vessels  
5 being arranged in parallel paths, flow control means to permit the feed gas to pass through each vessel and to the outlet assembly, a regeneration assembly comprising a conduit in fluid communication with the outlet assembly whereby a regeneration gas is able to be passed into each vessel and a heater to heat the regeneration gas, the flow control  
10 means and the regeneration assembly being arranged so that each vessel, in use, repeatedly undergoes an adsorption cycle comprising an adsorption step, depressurisation, a regeneration step and repressurisation and the adsorption cycle for each vessel is out of phase with the cycle for all the other vessels provided that, in use, at least two  
15 vessels are in the adsorption step at any time.

The present invention may be employed in combination with otherwise conventional air separation plant and other apparatus for gas separation. The invention also has applicability in other fields including remote applications, for example shipboard applications, where oxygen storage may be subject to safety  
20 scrutiny. The invention provides advantage in applications where continuous supply of a gas to a downstream process is important for economic, safety or other reasons. For example the need for reliability of supply of oxygen for a the downstream Fisher Tropsch or methanol production process is important and the present invention provides a safety benefit by being operable in a conventional  
25 mode, that is using a pair of beds in the event that the third vessel is inoperative for example in an emergency or due to scheduled process down-time.

Figure 1 shows a conventional cycle for the operation of a prior art two bed TSA process.

Figure 2 is a schematic illustration of apparatus according to the invention.

30 Figure 3 shows the cycle of operation of a process according to the invention and the apparatus of Figure 2.

In Figures 1 and 3, "D" denotes depressurisation, "R" denotes repressurisation and "REGEN" denotes regeneration. In Figure 1, a conventional TSA process cycle is shown in which the adsorbent in a first bed is on-line, receiving a feed gas and adsorbing at least one undesired component of the gas and the treated feed is then passed downstream, optionally for further processing. While the first bed is on line, the second bed is sequentially depressurised, regenerated by passing a regeneration gas through the bed counter-current to that of the feed gas when on-line and then repressurised. The regeneration gas is heated for at least the initial period of regeneration to provide a heat pulse which passes through the second bed and desorbs the adsorbed, undesirable component. Repressurisation of the second bed is then carried out. After repressurisation, the second bed is then switched to on-line operation and the first bed is taken off-line and subjected to the depressurisation, regeneration and repressurisation process.

A conventional TSA process typically has a cycle time of some hours whereas a conventional PSA process has a cycle time of the order of tens of minutes. Accordingly, use of downstream, treated gas to repressurise the bed undergoing regeneration does not adversely affect the continuity of the downstream flow to the same extent as in a PSA process.

Apparatus for use in accordance with the present invention shown in Figure 2 comprises three beds of adsorbent 1, 2 and 3 arranged in parallel. Each is connected via a respective inlet valve 4, 5 and 6 to an inlet manifold 7 connected to a source 8 of feed gas. The inlet end of each of the beds 1, 2 and 3 is also connected to a first venting manifold 9 via respective venting valves 10, 11 and 12. The outlet from each of the beds 1, 2 and 3 is connected via a respective outlet valve 13, 14 and 15 to an outlet manifold 16 which is connected to a downstream processing apparatus such as the cold box of an air separation unit 17. Regeneration gas for example from an air separation unit is supplied to the apparatus of Figure 2 at an input 18 via a heater 19 which is periodically switched on to provide a heated pulse of regeneration gas and is connected to the outlet end of each bed 1, 2 and 3 for counter-current purging flow via a respective inlet valves 20, 21 and 22. The outlets of the beds 1, 2 and 3 are interconnected

amongst themselves via valves 23, 24 and 25 to allow flow of repressurisation gas from outlet manifold 16. The operation of the control valves is controlled in a known manner by appropriate control means, not illustrated, but in a novel sequence to provide the phased adsorption cycles for the beds 1, 2 and 3.

5        The phasing of the operations of the beds 1, 2 and 3 is illustrated in Figure 3 which shows one adsorption cycle. It is this cycle which is repeated. In Figure 3 it can be seen that during the on-line or feed period of each bed, at least one of the other beds and is also on-line. Each bed is sequentially operated on-line, depressurised (D), regenerated and then repressurised (R). As the first bed 1 is  
10        taken off-line at  $t_a$ , the regenerated bed 2 is brought on-line, having been depressurised at  $t_c$ , regenerated and repressurised. During this time, the third bed 3 is on-line having been brought on-line at  $t_c$  during the adsorption step of the first bed 1 and is then taken off-line during the adsorption step of the second bed 2 at  $t_b$  after the first bed 1 is brought on-line. On being taken off-line, the first bed is  
15        then depressurised, regenerated and then repressurised and brought on-line at  $t_b$  at which time, the third bed is taken off-line and subjected to depressurisation, regeneration and repressurisation.

As one bed is taken off-line and another is brought on-line, a short period of overlap during which the two beds are both on-line is provided to allow for the  
20        mechanical opening and closing of valves.

The cycles of the beds suitably are phased so that there are overlaps for example of 10 to 20 seconds between the on-line periods of the beds. During such overlap periods, venting may be carried out to maintain a constant output of treated gas.

25        It will readily be appreciated that further beds may be included in parallel in a modified version of the apparatus shown in Figure 2.

The invention is illustrated by reference to the following non-limiting examples and the accompanying drawings.

#### Examples 1 to 6 and Comparative Examples A1 to A12

30        The effectiveness of a TSA system according to the invention as shown in Figure 2 with adsorption cycles phased as shown in Figure 3 and employing vertical beds was assessed by simulation.



Conventional processes were simulated according to the conventional TSA cycle shown in Figure 1 for operation with two beds and two pairs of beds where the beds are alternately on-line and off-line for comparative purposes.

Three sets of runs were simulated, at  $1000000 \text{ Nm}^{-2}$ ,  $600000 \text{ Nm}^{-2}$  and  
5  $300000 \text{ Nm}^{-2}$ .

Zeolite 13X of density  $640 \text{ kg/m}^3$ , was used as the adsorbent. Runs were simulated using small adsorbent beads and large adsorbent beads, altered, small beads being 1.0 to 2.4 mm in diameter and large beads being 2.4 to 5mm.

The molar purge to air ratio (P/A) was 0.15, contact time was set at 7  
10 seconds and the temperature of the feed gas at  $15^\circ \text{C}$ . The beds were taken to be 5m diameter. The approach to fluidisation of the bed was constant for runs at a given pressure and was less than 70%. A maximum regeneration temperature of  $140^\circ \text{C}$  was used.

The results are shown below in Tables 1 to 3.

15

Table 1 – Vertical bed at  $1000000 \text{ Nm}^{-2}$

Eg	Bead Size	No of Beds	Bed Height (m)	Air Flow ( $\text{Nm}^3/\text{h}$ )	DP, Pa/m (air)	DP, Pa/m (hot purge)
A1	SMALL	2	1.06	100,000	3533	2755
1	SMALL	3	1.06	200,000	3533	7073
A2	SMALL	4	1.06	200,000	3533	2755
A3	LARGE	2	1.06	150,000	3509	1687
2	LARGE	3	1.06	300,000	3509	5143
A4	LARGE	4	1.06	300,000	3509	1687

DP (air) refers to the pressure drop when operated on line and DP (hot purge) to the pressure drop during the regeneration step.

20

Table 2 – Vertical bed at 600000 Nm<sup>-2</sup>

Eg	Bead Size	No of Beds	Bed Height (m)	Air Flow (Nm <sup>3</sup> /h)	DP, Pa/m (air)	DP, Pa/m (hot purge)
A5	SMALL	2	1.4	80000	4000	2100
3	SMALL	3	1.4	160000	4000	5158
A6	SMALL	4	1.4	160000	4000	2100
A7	LARGE	2	1.4	120000	3830	1200
4	LARGE	3	1.4	240000	3830	3568
A8	LARGE	4	1.4	240000	3830	1200

Table 3 – Vertical bed at 300000 Nm<sup>-2</sup>

Eg	Bead Size	No of Beds	Bed Height (m)	Air Flow (Nm <sup>3</sup> /h)	DP, Pa/m (air)	DP, Pa/m (hot purge)
A9	SMALL	2	2.47	50000	3619	1183
5	SMALL	3	2.47	100,000	3619	2755
A10	SMALL	4	2.47	100,00	3619	1183
A11	LARGE	2	2.47	70,0000	2808	562
6	LARGE	3	2.47	140,000	2808	1518
A12	LARGE	4	2.47	140,000	2808	562

- 5 From the above results It can be seen that in Examples 1 to 6, by adding a third bed and operating the adsorption cycles out of phase a much higher air flow than a conventional two bed system and a comparable air flow as a conventional four bed system may be achieved. With three beds rather than four, major savings in capital and variable cost may be achieved.

10 Examples 7 and 8 and Comparative Examples B1 and B2

A series of simulations were carried out under the same conditions as set out under Examples 1 to 6 and A1 to A12 for a horizontal bed of 5m diameter and 2m depth. The pressure is 600000 Nm<sup>-2</sup>.

The results are shown in Table 4.

Table 4

Eg	Bead Size	No Beds	Air Flow (Nm <sup>3</sup> /h)	Bed Length (m)	DP, Pa/m (air)	DP, Pa/m (hot purge)
B1	SMALL	2	1000,000	34	3711	1515
7	SMALL	3	1000,000	16	3711	4379
B2	LARGE	2	1000,000	34	1711	571
8	LARGE	3	1000,000	17	1700	5391

Operating according to the present invention for a given air flow enables a horizontal bed of much shorter length to be employed than would be usable in a conventional process. Alternatively, for a given bed length, the present invention allows a significantly higher throughput to be achieved than a conventional process.

Example 9 and Comparative Example C1

A series of simulations were carried out under the same conditions as set out under Examples 1 to 6 and A1 to A12 for a radial bed of 5m diameter and 1.2m depth with a small bead size adsorbent. The pressure is 600000 Nm<sup>-2</sup>.

The results are shown in Table 5.

Eg	Air Flow (NM <sup>3</sup> /h)	Bed Length (m)	No Beds	DP, Pa/m (air)	DP, Pa/m (hot purge)
C1	1000,000	30	2	4180	2618
9	1000,000	15	3	4180	6828

Operating according to the present invention for a given air flow enables a radial bed of much shorter length to be employed than would be usable in a conventional process. Alternatively, for a given bed length, the present invention allows a significantly higher throughput to be achieved than a conventional process.

CLAIMS

1. A process for the reduction of the level of a component in a feed gas comprising passing the feed gas to at least three parallel thermal swing adsorption zones, each zone containing an adsorbent and being operated in an adsorption cycle which comprises an adsorption step to remove or to reduce the level of the component from the feed gas, depressurisation of the adsorption zone, a regeneration step to desorb the adsorbed component and repressurisation of the adsorption zone, wherein the adsorption cycle of each zone is phased with respect to that of the other zones so that at any point during the adsorption cycle, the number of zones in the adsorption step is greater than the number of zones not in the adsorption step.
2. A process as claimed in claim 1 in which the feed gas from which the undesired component has been removed is fed to a downstream cryogenic separation process.
3. A process as claimed in claim 1 or claim 2 in which the feed gas is selected from synthetic gas, natural gas and air.
4. A process as claimed in any one of the preceding claims in which the adsorbent is selected from alumina, silica gel, activated alumina, impregnated alumina, and a molecular sieve.
5. A process as claimed in any one of the preceding claims in which the undesired components comprise carbon dioxide and water and the adsorbent comprises a first adsorbent selected from silica gel, activated alumina, impregnated alumina and alumina and a second, downstream adsorbent comprising a zeolite.
6. A process as claimed in claim 5 in which the zeolite is selected from a zeolite of the X type, A type, LSX type having a silicon to aluminium ratio of 1.0 to 1.25.
7. A process as claimed in any one of the preceding claims in which the feed gas is at a temperature of  $-50$  to  $80^{\circ}\text{C}$ .

8. A process as claimed in claim 7 in which the feed gas is at a temperature of 5 to 50°C.
9. A process as claimed in any one of the preceding claims in which the regeneration of the adsorbent is carried out at a temperature of 0 to 400°C.
- 5 10. A process as claimed in any one of the preceding claims in which the adsorbent is regenerated by means of a regeneration gas and the molar ratio of regeneration gas to feed gas is 0.05 to 0.8.
11. A process as claimed in any one of the preceding claims in which the regeneration gas is at a pressure of 10000 to 2000000 N/m<sup>2</sup>.
- 10 12. A process as claimed in any one of the preceding claims in which the feed gas is at a pressure of at least 100000N/m<sup>2</sup>.
13. A process as claimed in claim 12 in which the feed gas is at a pressure of 200000 to 4000000 N/m<sup>2</sup>.
14. A process as claimed in any one of the preceding claims in which  
15 the feed gas is at a temperature of 5 to 50°C and a pressure of 200000 to 4000000 N/m<sup>2</sup>.
15. A process as claimed in any one of the preceding claims in which the feed gas comprises at least two independent feed gases, each gas having a different characteristic to the other gas(es).
- 20 16. A process as claimed in claim 16 in which the independent feed gases are at a different pressure on being fed to the adsorption cycle.
17. A process as claimed in any one of the preceding claims in which repressurisation of the an adsorption zone is effected by feeding to  
25 the zone a gas at higher pressure from upstream of the adsorption zone.
18. A process as claimed in any one of the preceding claims in which the adsorption cycle for all the adsorption zones is substantially the same duration.
- 30 19. A process as claimed in any one of the preceding claims in which the ratio of the duration of the adsorption step to the adsorption

cycle is not less than the ratio of one less than the number of adsorption zones to the number of adsorption zones.

20. A process as claimed in any one of the preceding claims having three adsorption zones.

5 21. A process as claimed in any one of the preceding claims in which the number of zones in the adsorption step at any point during the cycle is one fewer than the total number of adsorption zones.

22. A thermal swing adsorption apparatus for conducting thermal swing adsorption of a component in a feed gas, the apparatus comprising at least three parallel thermal swing adsorption zones adapted to receive an adsorbent bed and means for controlling the flow of the feed gas through the at least three zones such that each bed undergoes repeated adsorption cycles which cycle comprises an adsorption step to remove or to reduce the level of the component from the feed gas, depressurisation of the zone, a regeneration step to desorb the adsorbed component and repressurisation of the adsorption zone, and wherein the adsorption cycle of each zone is phased with respect to that of the other zones so that, in use, the number of zones in the adsorption step is greater than the number of zones not in the adsorption step.

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23. A thermal swing adsorption apparatus comprising at least three adsorption vessels, a feed gas inlet assembly in fluid communication with each vessel, an outlet assembly in fluid communication with the at least three vessels being arranged in parallel paths, flow control means to permit the feed gas to pass through each vessel and to the outlet assembly, a regeneration assembly comprising a conduit in fluid communication with the outlet assembly whereby a regeneration gas is able to be passed into each vessel and a heater to heat the regeneration gas, the flow control means and the regeneration assembly being arranged so that each vessel, in use, repeatedly undergoes an adsorption cycle comprising an adsorption step, depressurisation, a regeneration step and repressurisation and the

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adsorption cycle for each vessel is out of phase with the cycle for all the other vessels provided that, in use, at least two vessels are in the adsorption step at any time.

- 5        24. Apparatus as claimed in claim 22 or claim 23 in which the adsorption zone is defined by a vessel selected from a horizontal, vertical and radial bed vessel.
- 10       25. Apparatus as claimed in any one of claims 22 to 24 in which the means for controlling the flow of feed gas comprises conduits for gas flow in or connecting the zones and connecting each bed to a source of the feed gas and to an outlet from the apparatus for the gas treated by removal or reduction of the undesired component, valve means in the conduits operable to open and close respective ones of the conduits.
- 15       26. Apparatus as claimed in any one of claims 22 to 25 in which the means for controlling the flow of gas comprises valve control means programmed to operate the valve means in sequence to produce the required adsorption cycles of operation.
27. Use of apparatus as claimed in any one of claims 22 to 26 in a process as defined in any one of claims 1 to 21.